

04-CHEM-A4, CHEMICAL REACTOR ENGINEERING

MAY 2015

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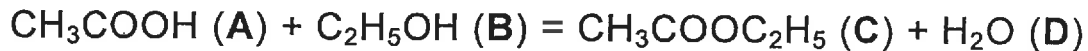
3 hours Duration

1. If doubt exists as to the interpretation of any question, please submit with your answer a clear statement of any assumption(s) you make. If possible, please underline or enclose any such statement in a box.
2. This is an OPEN BOOK EXAM. You may bring to this exam
 - the official designated textbook by Fogler – any edition – annotated in margins, etc. as desired. No loose notes allowed.
 - your own unit conversion tables and/or mathematical tables such as a CRC Handbook.
 - a non-communicating, programmable electronic calculator using a small operating guide. Please write the name and model of your calculator on the first inside left-hand sheet of the exam workbook.
3. Graph paper will be provided.
4. Any **four** questions constitute a complete paper and, unless you indicate otherwise, only the first four answers as they appear in your answer booklet will be marked.
5. Each question is worth 20 points. Marking schemes are provided in brackets after each question.
6. Technical content is the key ingredient in your answers. However, no credit will be given for deriving rate expressions, or standard formulas that are available in the textbook. Clear writing is essential, particularly when explanations are required.
7. It will help the examiner if you could cite the origin of significant formula used – e.g., Fogler, eq. (3-44).

Marking Scheme – Four questions comprise a complete exam.

1. 20 points
2. 20 points
3. 20 points – a) 10 points, b) 10 points
4. 20 points
5. 20 points

Ethyl acetate ($\text{CH}_3\text{COOC}_2\text{H}_5$) is to be manufactured by the esterification of acetic acid (CH_3COOH) with ethanol ($\text{C}_2\text{H}_5\text{OH}$) in an isothermal batch reactor as shown below:



A production rate of 10,000 kg/day of ethyl acetate is required. The reactor will be charged with a mixture containing 500 kg/m³ ethanol, 250 kg/m³ acetic acid, the remainder being water, and very small quantity of hydrochloric acid as a catalyst. The density of this mixture is 1045 kg/m³, which will be assumed constant throughout the reaction. The reaction is reversible with a rate equation given by

$$r_A = k_f C_A C_B - k_r C_C C_D$$

At the operating temperature of 100 °C, the rate constants have the following values:

$$k_f = 8 \times 10^{-6} \text{ m}^3/\text{kmol}\cdot\text{s}$$

$$k_r = 2.7 \times 10^{-6} \text{ m}^3/\text{kmol}\cdot\text{s}$$

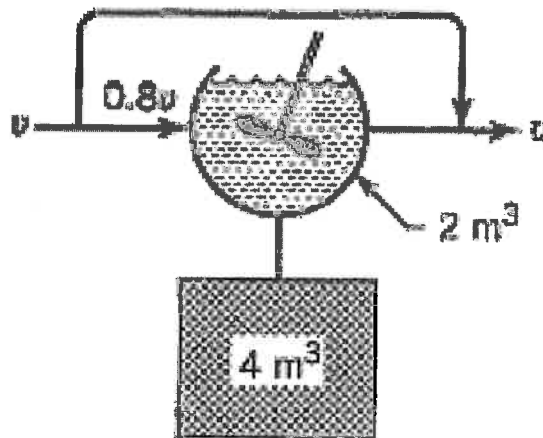
The reaction mixture will be discharged when the conversion of acetic acid is 30%. A time of 30 minutes is required for discharging, cleaning, and recharging. Determine the volume of reactor required.

QUESTION 2

The second order aqueous reaction

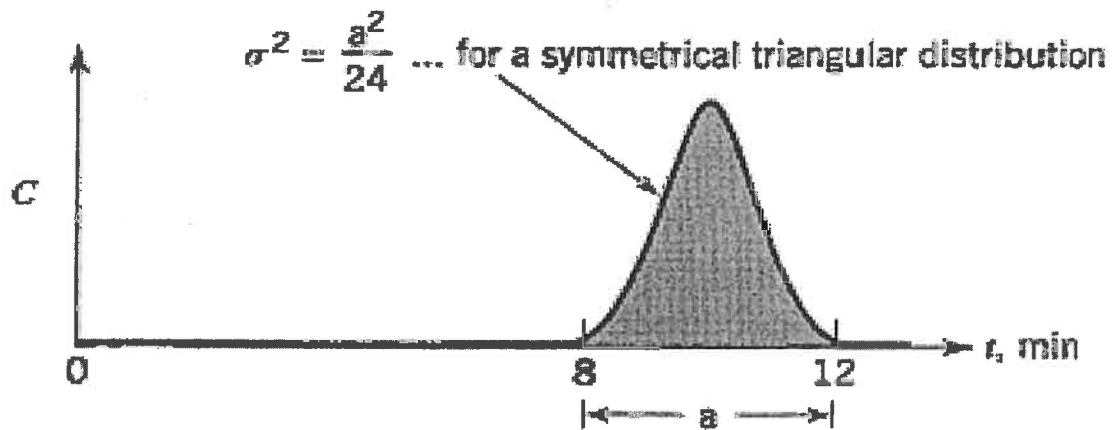


is run in a large tank reactor ($V = 6 \text{ m}^3$) and for an equimolar feed stream ($C_{A0} = C_{B0}$) conversion of reactants is 60%. Unfortunately, agitation in the reactor is rather inadequate and tracer tests of the flow within the reactor give the flow model shown below which includes a 4 m^3 dead zone:



What size of mixed flow reactor will equal the performance of the unit shown?

Calculations show that a plug flow reactor would give 99.9% conversion of reactant, which is in aqueous solution. However, the reactor has a residence time distribution as shown in the figure below:



The variance for a symmetrical triangle with base “a” rotating about its centre of gravity is given by $\sigma^2 = a^2/24$

- (a) If $C_{A0} = 1000$, what outlet concentration can we expect in the reactor for a first order reaction?
- (b) Repeat part (a) using the tanks-in-series model.

QUESTION 4

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Laboratory experiments on an irreversible, homogeneous gas-phase reaction



have shown the reaction rate constant to be $1 \times 10^5 \text{ L}^2/\text{mol}^2\cdot\text{s}$ at 500°C . Analysis of isothermal data from this reaction has indicated that a rate expression of the form

$$-r_A = kC_A C_B^2$$

provides an adequate representation for the data at 500°C and 1 atm total pressure. Calculate the volume of an isothermal, isobaric plug-flow reactor that would be required to process 6 L/s of a feed gas containing 25% A, 25% B, and 50% inerts by volume for a fractional conversion of 90% of component A.

Kinetic experiments on the solid catalyzed reaction



are conducted at 8 atm and 700 °C in a mixed reactor 960 cm³ in volume and containing 1 gram of catalyst of diameter $d_p = 3$ mm. Feed consisting of pure A is introduced at various rates into the reactor and the partial pressure of A in the exit stream is measured for each feed rate as shown below:

Volumetric Feed Rate, V_0 (in liters per hour)	Partial Pressure $p_{A,out}/p_{A,in}$
100	0.8
22	0.5
4	0.2
1	0.1
0.6	0.05

Find a rate equation to represent the rate of reaction on catalyst of this size.

The Periodic Table of the Elements

Hydrogen 1 H 1.01	2 He 4.00																
Lithium 3 Li 6.94	Beryllium 4 Be 9.01																
Sodium 11 Na 22.99	Magnesium 12 Mg 24.31																
Potassium 19 K 39.10	Calcium 20 Ca 40.08																
Rubidium 37 Rb 85.47	Strontium 38 Sr 87.62																
Cesium 55 Cs 132.91	Barium 56 Ba 137.33																
Francium 87 Fr (223)	Radium 88 Ra (226)																
<div style="display: flex; justify-content: space-between; align-items: center;"> <div style="text-align: center;"> <p>Alkali metals</p> <p>Alkaline earth metals</p> <p>Transition metals</p> <p>Other metals</p> <p>Metalloids (semi-metal)</p> <p>Nonmetals</p> <p>Halogens</p> <p>Noble gases</p> </div> <div style="text-align: center;"> <p>Element name → Mercury</p> <p>80</p> <p>Symbol → Hg</p> <p>Avg. Mass ← 200.59</p> </div> </div>																	
Atomic # ←																	
Avg. Mass ←																	
			13			14			15			16			17		
			Boron			Carbon			Nitrogen			Oxygen			Fluorine		
			5			6			7			8			9		
			B			C			N			O			F		
			10.81			12.01			14.01			16.00			19.00		
			Aluminum			Silicon			Phosphorus			Sulfur			Chlorine		
			13			14			15			16			17		
			Al			Si			P			S			Cl		
			26.98			28.09			30.97			32.07			35.45		
			Gallium			Germanium			Arsenic			Selenium			Bromine		
			31			32			33			34			35		
			Ga			Ge			As			Se			Br		
			69.72			72.61			74.92			78.96			79.90		
			Indium			Tin			Antimony			Tellurium			Iodine		
			49			50			51			52			53		
			In			Sn			Sb			Te			I		
			114.82			118.71			121.76			127.60			126.90		
			Thallium			Lead			Bismuth			Polonium			Astatine		
			81			82			83			84			85		
			Tl			Pb			Bi			Po			At		
			204.38			207.20			208.98			(209)			(210)		
			Ununquadium			Ununhexium			Ununseptium			Ununhassium			Ununseptium		
			113			114			115			116			117		
			Uut			Uuq			Uup			Uuh			Uus		
			(284)			(289)			(288)			(293)			(294?)		

Lanthanum 57 La 138.91	Cerium 58 Ce 140.12	Praseodymium 59 Pr 140.91	Neodymium 60 Nd 144.24	Promethium 61 Pm (145)	Samarium 62 Sm 150.36	Europium 63 Eu 151.97	Gadolinium 64 Gd 157.25	Dysprosium 66 Dy 162.50	Terbium 65 Tb 158.93	Ytterbium 70 Yb 173.04
Actinium 89 Ac (227)	Thorium 90 Th 232.04	Protactinium 91 Pa 231.04	Uranium 92 U 238.03	Neptunium 93 Np (237)	Plutonium 94 Pu (244)	Americium 95 Am (243)	Curium 96 Cm (247)	Californium 98 Cf (251)	Mendelevium 101 Md (258)	Nobelium 102 No (259)

*lanthanides

**actinides

